### <u>Outline</u>

- Corrosion Introduction
- Corrosion of Metals
  - e.g. Rusting of iron in water
- Electrochemical Cell
- Electrode Potential in Electrochemical Cell
- Standard Electromotive Force
- Example
- Relative Corrosion Potential
- Oxidation or Dry Corrosion
- Degradation of Polymers



# **CORROSION of Metals**

## **ISSUES TO ADDRESS...**

- Why does corrosion occur?
- What metals are most likely to corrode?
- How do temperature and environment affect corrosion rate?
- How do we suppress corrosion?

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## **CORROSION**

### • Corrosion:

Is the destruction of a material due to electrochemical attack from the environment.





### • Cost:

- ➤ 4 to 5% of the Gross National Product (GNP)
- > 2.5 trillion USD global cost of corrosion 2016 estimate
- In USA, this amount is about \$400 billion/yr



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## **CORROSION**

- Corrosion depends on:
  - chemicals present
  - type of material (metal, ceramic, polymer)
  - temperature
  - exposure time
  - stress .... etc

### Type of material and corrosion

- Metals
  - tend to dissolve (Corrosion)
  - form non-metallic film (Oxidation)
- Ceramics
  - relatively inert, but under certain conditions corrosion may occur.
- Polymers

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- may dissolve in solvents, swell, UV - degradation.

# **CORROSION OF METALS**

- Most metals naturally occur as ceramics, (oxides, sulphides etc).
- Metal is extracted from ore (using considerable energy), and then used as metal or alloy.
- But as metals are usually in higher energy state, more favourable energetically, to reform oxides etc.

Occasionally corrosion process is useful:

- aluminum oxide (anodizing)
- etching of microstructures.
- dry-cell batteries

#### BUT usually it is **undesirable**



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# CORROSION OF METALS

Corrosion of metals takes place through ...... process where: • Oxidation - reduction processes take place and metal atoms lose electrons (become ions) and go into solution.

Often occurs in aqueous medium where moisture can provide electrical circuit to form an *electrochemical cell*.

### **OXIDATION REACTION** (occurs at the ANODE) - Corrosion (dissolving)

Metals  $\rightarrow$  Ions

 $M \rightarrow M^{n+} + n e^{-}$ 

i.e. Metal anode dissolves.

e.g.:  $Zn \rightarrow Zn^{2+} + 2e^{-}$ Na  $\rightarrow$  Na<sup>1+</sup> + 1e<sup>-</sup> Fe  $\rightarrow$  Fe<sup>2+</sup> + 2e<sup>-</sup>

#### Electrons transferred to another chemical reaction - Reduction

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# **CORROSION OF METALS**

**REDUCTION reactions** (occur at the cathode - Cathodic Reaction)

- These depend on what is available:
  - ✓ If H<sup>+</sup> ions are available then:  $2H^+ + 2e^- \rightarrow H_2$
  - ✓ If acid solution with dissolved oxygen:  $O_2 + 4H^+ + 4e^- \rightarrow 2H_2O$
  - ✓ If basic/neutral with dissolved oxygen:  $O_2 + 2H_2O + 4e^- \rightarrow 4(OH^-)$
- If some metal ions are present they may be reduced by the electrons:

 $M^{n+} + n e^{-} \rightarrow M$  (*electroplating*) or  $M^{n+} + e^{-} \rightarrow M^{(n-1)+}$ 

Can get more than one of these occurring at the same time



# CORROSION OF METALS

The overall electrochemical reaction consists of at least one oxidation reaction (half-reaction) and at least one reduction half-reaction.

Total oxidation = total reduction (charge balance)





# Electrochemical cell



- The cathode receives electrons from the circuit by means of a chemical or cathode reaction. Byproducts may form.
- The anode and cathode must be electrically connected (usually by physical contact).
- A liquid electrolyte must be in contact with the anode and cathode to <u>complete the circuit</u> and allow movement of ions.





## Electrode Potential In Electrochemical Cells

➢ For perfect metal in an electrolyte, an Electrode Potential is developed which is related to the tendency of the metal to give up electrons (oxidise).

> *Different metals* have <u>different</u> tendencies to be oxidised.

<u>Example</u>: If iron and copper electrodes in their respective ions are connected electrically:

- iron electrode will dissolve (oxidise) Fe
- $\rightarrow$  Fe<sup>2+</sup> + 2e<sup>-</sup> and

• copper electrode will grow (electroplate –  $Cu^{2+}$  be reduced)  $Cu^{2+} + 2e^- \rightarrow Cu$  giving in total:  $Fe + Cu^{2+} \rightarrow Fe^{2+} + Cu$ 



#### A voltage difference of 0.78V is associated with this reaction.

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## Electrode Potential In Electrochemical Cells



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Standard Electrode Potential

Electrode Potential In Electrochemical Cells



# Standard Electromotive Force (EMF) Series

#### Table 18.1 The Standard emf Series

For any given metal say		Electrode Reaction	Standard Electrode Potential, V <sup>®</sup> (V)
$Fe^{2+}$ anything above it on		$Au^{3+} + 3e^{-} \longrightarrow Au$	+1.420
the table would get as a	Î	$O_2 + 4H^+ + 4e^- \longrightarrow 2H_2O$	+1.229
the table would act as a		$Pt^{2+} + 2e^- \longrightarrow Pt$	~+1.2
<i>cathode</i> relative to the iron		$Ag^+ + e^- \longrightarrow Ag$	+0.800
and cause it to corrode	Increasingly inert	$Fe^{3+} + e^{-} \longrightarrow Fe^{2+}$	+0.771
	(cathodic)	$O_2 + 2H_2O + 4e^- \longrightarrow 4(OH^-)$	+0.401
Similarly, anything listed		$Cu^{2+} + 2e^{-} \longrightarrow Cu$	+0.340
below iron would act as an		$2H^+ + 2e^- \longrightarrow H_2$	0.000
anode relative to iron and		$Pb^{2+} + 2e^- \longrightarrow Pb$	-0.126
undue relative to from and		$Sn^{2+} + 2e^{-} \longrightarrow Sn$	-0.136
cause it to plate out.		$Ni^{2+} + 2e^{-} \longrightarrow Ni$	-0.250
		$Co^{2+} + 2e^{-} \longrightarrow Co$	-0.277
		$Cd^{2+} + 2e^{-} \longrightarrow Cd$	-0.403
To find the net emf for any		$Fe^{2+} + 2e^{-} \longrightarrow Fe$	-0.440
	Increasingly active	$Cr^{3+} + 3e^{-} \longrightarrow Cr$	-0.744
given pair of electrodes,	(anodic)	$Zn^{2+} + 2e^{-} \longrightarrow Zn$	-0.763
simply take the difference		$Al^{3+} + 3e^{-} \longrightarrow Al$	-1.662
hetween the values listed		$Mg^{2+} + 2e^{-} \longrightarrow Mg$	-2.363
between the values listen.	Į	$Na^+ + e^- \longrightarrow Na$	-2.714
	•	$K^+ + e^- \longrightarrow K$	-2.924

These are for the reduction reactions; for the oxidation reactions, the direction of the reaction is reversed and the sign of the voltage changed.

#### Example: .....

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## Reaction's Direction

#### Example:

Metal M <sub>1</sub>	is oxidised	and M	1etal M <sub>2</sub>	is	reduced	thus:	
1							

 $M_1 \rightarrow M_1^{n+} + ne^{-}$  $-V_{1}^{0}$ (opposite sign to Table)

 $M_2^{n+} + ne^- \rightarrow M_2$  $+V^{0}$ 

Addition of equations yields:  $M_1 + M_2^{n+} \rightarrow M_1^{n+} + M_2$ 

and the overall cell potential is:  $\Delta V^0 = V_2^0 - V_1^0$ 

If this value ( $\Delta V^0$ ) is +ve then reaction occurs spontaneously.

If it is negative, the reaction will go the other way.

Remember: When standard half-cells are coupled together, the metal that is lower in the Standard EMF series will oxidize (corrode) and the other will be reduced (electro-deposit).

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## Relative corrosion potential

• Since the preceding table was constructed under highly idealized conditions, it is sometimes more useful to rank the metals according to their general tendency to corrode in seawater.

• Metals near the top are ..... cathodic (meaning that they resist corrosion and accept electrons), whereas metals near the bottom corrode rather easily and act as a source of electrons.

• If metal "A" falls below metal "B" on this list, "A" will most likely corrode and eventually disintegrate when electrically connected to "B"

Table 18.2 The Galvanic S	Series
	Platinum
	Gold
	Graphite
	Titanium
	Silver
	[316 Stainless steel (passive)
	304 Stainless steel (passive)
t	[Inconel (80Ni-13Cr-7Fe) (passive)
	Nickel (passive)
	[Monel (70Ni-30Cu)
Increasingly inert (cathodic)	Copper-nickel allovs
0. ( )	Bronzes (Cu-Sn allovs)
	Copper
	Brasses (Cu-Zn alloys)
	[Inconel (active)
	Nickel (active)
	Tin
	Lead
Increasingly active (anodic)	[316 Stainless steel (active)
	304 Stainless steel (active)
	Cast iron
1	Iron and steel
	Aluminum allovs
	Cadmium
	Commercially pure aluminum
	Zinc
	Magnesium and magnesium alloys



### Oxidation – Dry Corrosion

Degradation of metals in gaseous atmosphere (usually air) by reaction of surface. (scaling, tarnishing, dry corrosion) - Also an electrochemical process

$$\begin{split} M &\to M^{2+} + 2e^{-} \\ \frac{1}{2} O_2 + 2e^{-} \to O^{2-} \end{split}$$
oxidation reduction

Overall

The important issue when it comes

to oxidation is whether the oxide layer keeps growing after or not. In

order for this to happen, oxidising

species must diffuse through the

oxide layer.



 $M + \frac{1}{2}O_2 \rightarrow MO$ 



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## **Oxidation Rate**

### Rate of oxidation (oxide layer growth rate) is related to the relative volumes:

 $P - B Ratio = \frac{A_o.\rho_M}{A_M.\rho_o}$ 

Where A is molecular weight

P-B is Pilling-Bedworth Ratio

ρ density M denotes metal and O oxide. (based on Volume = Mass/Density)

Table 17.3

Ce

Al

Pb

Ni

Be

Pd

Cu

Fe

Mn

Co

Cr

Si

Protective

1.16

1.28

1.40

1.52

1.59

1.60

1.68

1.77

1.79

1.99

1.99

2.27

- For P-B ratio less than 1, oxide film tends to be non-protective and porous and doesn't fully cover the surface.
- For P-B ratio greater than 1, compressive stresses form in oxide film (tend to be protective).
- For P-B ratio greater than 2-3, oxide film may crack and flake off exposing fresh metal (tend to be non-protective).
- This is based on volume change but other factors apply as well

3.6	TC	TTP	0	$\sim$	1
13/1	ы.	н	- 1	1	
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**Pilling-Bedworth Ratios** 

Κ

Li

Na

Cd

Ag

Ti

Ta

Sb

Nb

U

Mo

W

for a Number of Metals

Nonprotective

0.45

0.57

0.57

1.21

1.59

1.95

2.33

2.35

2.61

3.05

3.40

3.40



## Kinetics of Oxidation

## $W^2 = K_1 t + K_2$

Rate measured by weight gain per unit area (W) as a function of time (t).

- ✓ For non-porous, well-attached oxide, growth is related to ionic diffusion giving a parabolic rate,  $(K_1 \text{ and } K_2 \text{ are constants for a given temperature})$ . - Examples: iron, cobalt, copper
- ✓ For porous, flaky oxide, growth is usually linear. - Examples: Na, K, Ta

#### $W = K_3 t$

✓ For some very thin oxide films, growth at low temperatures can be logarithmic. - Examples: Al, Fe, Cu at ambient temperature

$$W = K_4 \log(K_5 t + K_6)$$

Linear Paraboli Logarithmic Time, t

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### **Degradation of Polymers**

- Not electrochemical corrosion. (Physio-chemical)
  - Swelling and degradation, bond rupture are some common mechanisms. 2
  - Liquid/solute diffuses into polymer and between large molecules. 2 Swells polymer making it weaker.

Material	Weather- Sunlight Aging	Oxidation	Ozone Cracking	Alkali Dilute/ Concentrated	Acid Dilute/ Concentrated	Chlorinated Hydrocarbons, Degreasers	Aliphatic Hydrocarbons, Kerosene, Etc.	Animal, Vegetable Oils
Polvisoprene	00							
(natural)	D	в	NR	A/C-B	A/C-B	NR	NR	D-B
Polyisoprene								
(synthetic)	NR	в	NR	C-B/C-B	C-B/C-B	NR	NR	D-B
Butadiene	D	в	NR	C-B/C-B	C-B/C-B	NR	NR	D-B
Styrene-								
butadiene	D	С	NR	C-B/C-B	C-B/C-B	NR	NR	D-B
Neoprene	в	A	A	A/A	A/A	D	С	B
Nitrile (high)	D	в	С	B/B	B/B	C-B	А	в

Table 17.5 Resistance to Degradation by Various Environments for Selected Elastomeric Materials<sup>a</sup>

<sup>a</sup> A = excellent, B = good, C = fair, D = use with caution, NR = not recommended.

Α

А

Source: Compound Selection and Service Guide, Seals Eastern, Inc., Red Bank, NJ, 1977.

(polysiloxane) A

B/C

NR

A/A

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Α

D-C



### **Degradation of Polymers**

Resistance to Degradation by Various Environments for Selected Plastic Materials<sup>a</sup> Table 17.4

Material	Nonoxidizing Acids (20% H <sub>2</sub> SO <sub>4</sub> )	Oxidizing Acids (10% HNO <sub>3</sub> )	Aqueous Salt Solutions (NaCl)	Aqueous Alkalis (NaOH)	Polar Solvents (C <sub>2</sub> H <sub>5</sub> OH)	Nonpolar Solvents (C <sub>6</sub> H <sub>6</sub> )	Water
Polytetrafluoro-							
ethylene	S	S	S	S	S	S	S
Nylon 6,6	U	U	S	S	Q	S	S
Polycarbonate	Q	U	S	U	S	U	S
Polyester	Q	Q	S	Q	Q	U	S
Polyetherether-							
ketone	S	S	S	S	S	S	S
Low-density polyethylene	S	Q	s	122	S	Q	s
High-density polyethylene	S	Q	S	-	S	Q	s
Poly(ethylene terephthalate)	S	Q	s	s	s	s	s
Poly(phenylene oxide)	S	0	s	s	S	U	S
Polypropylene	S	Q	S	S	S	0	S
Polystyrene	S	õ	S	S	S	Ü	S
Polyurethane	0	Ũ	S	0	U	0	S
Epoxy	S	Ū	S	S	S	S	S
Silicone	Q	U	S	S	S	Q	S

<sup>a</sup>S = satisfactory; Q = questionable; U = unsatisfactory.

Source: Adapted from R. B. Seymour, Polymers for Engineering Applications, ASM International, Materials Park, OH, 1987.

Next time: Continue Corrosion

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