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Why Plastic Shaping Processes are Important

- Applications of plastics have increased at a much faster rate than ٠ either metals or ceramics during the last 50 years
 - Many parts previously made of metals are now being made of plastics
 - For example: plastic containers have been largely substituted for glass *bottles and jars*
- Total volume of polymers (plastics and rubbers) now that of metals (tonnage is still less because density of metals is greater)
- Almost unlimited variety of part geometries ٠
- Plastic molding is a process; further shaping is not needed ٠
- Less energy is required than for metals because processing • temperatures are much lower
 - Handling of product is simplified during production because of lower temperatures
- Painting or plating is usually not required



Two Types of Plastics

1. Thermoplastics

- _ *Chemical structure remains unchanged during heating and shaping*
- More important commercially, comprising more than 70% of total _ plastics tonnage
- 2. Thermosets
 - Undergo a curing process during heating and shaping, causing a _ permanent change (called cross-linking) in molecular structure
 - Once cured, they cannot be remelted _
- To shape a thermoplastic polymer it must be heated so that it \checkmark softens to the consistency of a liquid
- In this form, it is called a *polymer melt* \checkmark
- Important properties:
 - Viscosity _
 - Viscoelasticity _

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Viscosity of Polymer Melts

Fluid property that relates shear stress to shear rate during flow

- Due to its high molecular weight, a polymer melt is a thick fluid with high viscosity
- Important because most polymer shaping processes involve flow through small channels or die openings
- Flow rates are often, leading to high shear rates and shear stresses, so significant pressures are required to accomplish the processes



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Viscosity of Polymer Melts





Viscoelasticity

Combination of viscosity and elasticity

- Possessed by both polymer solids and polymer melts
- Example: die swell in extrusion, in which the hot plastic expands when exiting the die opening







- Compression process in which material is forced to flow through a die orifice to provide long continuous product whose cross-sectional shape is determined by the shape of the orifice
- Widely used for thermoplastics and elastomers to mass produce items such as tubing, pipes, hose, structural shapes, sheet and film, continuous filaments, and coated electrical wires
- Carried out as a continuous process; *extrudate* is then cut into desired lengths ٠

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Two Main Components of an Extruder

Screv

1- Barrel

 Internal diameter typically ranges from 25 to 150 mm

• L/D ratios usually between 10 and 30: ratios for thermoplastic, ratios for elastomers

• Electric heaters melt feedstock; subsequent mixing and mechanical working adds heat which maintains the melt

2- Screw

Divided into sections to serve several functions:

- Feed section - feedstock is moved from hopper and preheated

- Compression section - polymer is transformed into fluid, air mixed with pellets is extracted from melt, and material is compressed

- Metering section - melt is homogenized and sufficient pressure developed to pump it through die opening

Die - not an extruder component (It is a special tool that must be *fabricated for particular profile to be produced*)

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- Functions of screen pack:
 - Filter contaminants and hard lumps from melt
 - Build pressure in metering section
 - Straighten flow of polymer melt and **remove its** "memory" of circular motion imposed by screw

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Common die profiles and corresponding extruded shapes:

Extrusion die

Extrudate

profile

- Solid profiles
- Hollow profiles, such as tubes
- Wire and cable coating
- Sheet and film
- Filaments

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Extruding Hollow Profiles Breaker plate



- ٠ Examples: tubes, pipes, hoses, and other cross-sections containing holes
- Hollow profiles require mandrel to form the shape
- Mandrel held in place using a spider ٠
 - Polymer melt flows around legs supporting the mandrel to reunite into a monolithic tube wall
- Mandrel often includes an air channel through which air is blown to ٠ maintain hollow form of extrudate during hardening



Melt Flow in Extruder

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- As screw rotates inside barrel, polymer melt is forced to move forward toward die; as in an screw
- Principal transport mechanism is *drag flow*, Q_d , resulting from friction between the viscous liquid and the rotating screw
- Compressing the polymer melt through the die creates a back pressure that reduces drag flow transport (called *back pressure flow*, $Q_{\rm b}$)
- Resulting flow in extruder is $Q_x = Q_d Q_h$



Direction of melt flow

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Wire and Cable Coating

Direction of melt flow • Polymer melt is applied to Vertical extruder barrel bare wire as it is pulled at high Screen pack speed through a die • • A slight vacuum is drawn between wire and polymer to thermoforming Polymer melt Breaker plate promote adhesion of coating • Wire provides rigidity during Die sections Core tube Film: Coated wire out cooling - usually aided by Bare wire in passing coated wire through a water trough Vacuum seal • Product is wound onto large bags) spools at speeds up to 50 m/s Partial vacuum drawn ٠ ditches Mech 421/6511 lecture 15/13 Mech. Eng. Dept. - Concordia University Dr. M. Medraj Slit-Die Extrusion of Sheet and Film Section A-A Direction of melt flow Section B-B Manifold thin film Manifold Extruded film mandrel Slit may be up to 3 m wide and as narrow as around 0.4 mm ٠ A problem in this method is of thickness throughout width of stock, due to drastic shape change of polymer melt during its flow



Polymer Sheet and Film

Sheet:

- Thickness from 0.5 mm to ~12.5 mm Materials for Polymer Sheet and Film:
- Used for products such as flat window glazing and stock for
- Thickness below 0.5 mm
- Used for packaging (product wrapping material, grocery bags, and garbage
- Thicker film applications include pool covers and liners for irrigation

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All thermoplastic polymers
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- Polyethylene, mostly low density PE
- Polypropylene
- Polyvinylchloride - Cellophane

Processes include:

• Slit-Die Extrusion of Sheet and Film

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- Blown-Film Extrusion Process
- Calendering

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- through die
- Edges of film usually must be trimmed because of thickening at edges

Blown-Film Extrusion Process

- Combines extrusion and blowing to produce a tube of
- Process begins with extrusion of tube that is drawn upward while still molten and simultaneously expanded by air inflated into it through die
- Air is blown into tube to maintain uniform film thickness and tube diameter



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Calendering

- Feedstock is passed through a series of rolls to reduce thickness to desired gage
- Equipment is, but production rate is high
- Process is noted for surface finish and high gage accuracy
- <u>Typical materials:</u> rubber or rubbery thermoplastics such as plasticized PVC
- <u>Products:</u> PVC floor covering, shower curtains, vinyl table cloths, pool liners, and inflatable boats and toys





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Spinneret

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Fiber and Filament Products

Most important application of fibers and filaments is in textiles Feed honne Their use as reinforcing materials in Heating uni olymer mel plastics (composites) is growing, but Pump still small compared to textiles • Definitions: Molten draw region Fiber - a long, thin strand whose length is at least 100 times its diameter Solidification Filament - a fiber of continuous length Fibers can be natural or synthetic Synthetic fibers constitute about 75% of total fiber market today: - Polyester is the most important - Others: nylon, acrylics, and rayon Natural fibers are about 25% of total: Yarn driving ro - Cotton is by far the most important Wool production is less than cotton Mech 421/6511 lecture 15/18 Dr. M. Medraj Mech. Eng. Dept. - Concordia University



Melt Spinning

- Starting polymer is heated to molten state and pumped through spinneret, similar to conventional extrusion
 Pumo
 Pumo
- Typical spinneret is 6 mm thick and contains approximately 50 holes of diameter 0.25 mm
- Filaments are drawn and air cooled solidification before being spooled onto bobbin
- Significant extension and thinning of filaments occur while polymer is still molten, so final diameter wound onto bobbin may be only 1/10 of extruded size
- Used to produce filaments of polyesters and nylons



Polymer granules



Dry Spinning

- Similar to melt spinning, but starting polymer is in solution and solvent can be separated by evaporation
- First step is extrusion through spinneret
- Extrudate is pulled through a heated chamber which removes the solvent, leaving the polymer
- Used to produce filaments of cellulose acetates and acrylics

Wet Spinning

- Polymer is also in solution, only solvent is non-volatile
- To separate polymer, extrudate is passed through a liquid chemical that coagulates or precipitates the polymer into coherent strands which are then collected onto bobbins
- Used to produce filaments of rayon (regenerated cellulose)

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Subsequent Processing of Filaments



- Filaments produced by any of the three processes are usually subjected to further cold drawing to align crystal structure along direction of filament axis
 - Extensions of 2 to 8 are typical
 - Effect is to significantly increase tensile strength
 - Drawing is accomplished by pulling filament between two spools, where winding spool is driven at a faster speed than unwinding spool



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